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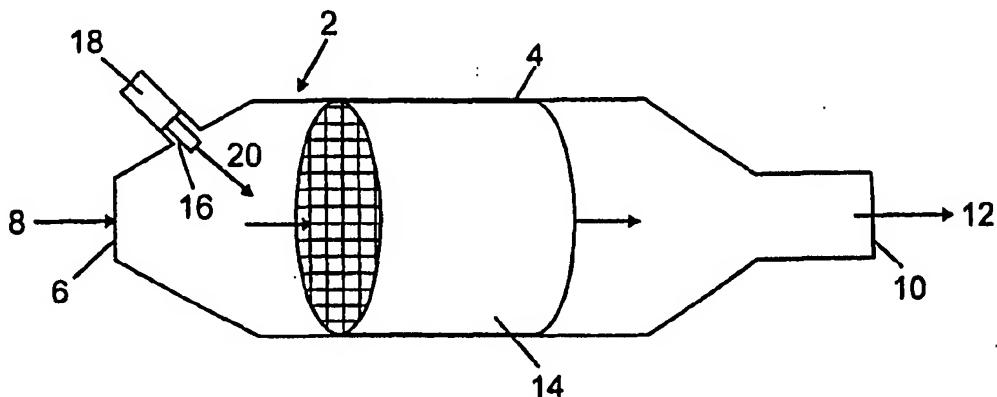
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(54) Title: REDUCTION OF NITROGEN OXIDES IN DIESEL EXHAUST GASES AND FUEL INJECTION SYSTEM



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(57) Abstract: A method for reducing NO<sub>x</sub> in lean exhaust gases (8) to N<sub>2</sub> includes injecting a fuel (20) into the exhaust gases (8) and passing the exhaust gases and fuel mixture through a catalyst (14) to reduce the NO<sub>x</sub> to N<sub>2</sub>. The catalyst (14) may be (a) a perovskite compound, (b) at least one metal oxide impregnated with at least one precious metal, (c) a zeolite impregnated with at least one precious metal, or (d) a combination of a zeolite and at least one metal oxide impregnated with at least one precious metal.

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## REDUCTION OF NITROGEN OXIDES IN DIESEL EXHAUST GASES AND FUEL INJECTION SYSTEM

### BACKGROUND OF THE INVENTION

5        Nitrogen oxides (NO<sub>x</sub>) in the earth's atmosphere are primarily emitted by  
automobiles and industrial plants. Studies have shown that nitrogen oxides can be  
hazardous to human health and the environment when present in the atmosphere in  
sufficiently high concentrations. For instance, nitrogen oxides above 0.05 ppm can  
have hazardous effects on people in good health for an exposure of over 24 hours. See,  
10      Fritz, A. and Pitchon, V., "The current state of research on automotive lean NO<sub>x</sub>  
catalysts," Applied Catalysis B: Environmental, Vol. 13 (1997), pp. 2. In particular,  
nitrogen oxides have been found to provoke lung infection and respiratory allergies.  
Nitrogen oxides have also been found to play an influential role in the formation of acid  
rain, smog, and general atmospheric visibility degradation. Because of the potential  
15      detrimental effects of nitrogen oxides on human health and the environment, the  
government has imposed several stringent regulations on NO<sub>x</sub> emissions. These  
tightened regulations continue to drive NO<sub>x</sub> abatement technology.

20      Several technologies have been developed in order to decrease NO<sub>x</sub> emissions,  
including passive methods using catalysts and active approaches such as  
electrochemical catalysis, photocatalytical approaches, plasma, laser, and so forth.  
Rich-burning engines, such as those used in today's gasoline-powered automobiles, use  
a three-way catalyst to reduce NO<sub>x</sub> emissions. The three-way catalyst typically consists  
of a combination of noble metals deposited on a stabilized alumina carrier. The three-  
way catalyst is efficient because it works together with a feedback system that directs  
25      the engine to blend air and fuel in stoichiometric proportions. By controlling the air-to-  
fuel ratio, the engine makes hydrocarbons and carbon monoxide available in just the  
right amounts to reduce NO<sub>x</sub> and unburned hydrocarbons to products like carbon  
dioxide, water, hydrogen gas, and nitrogen gas that are generally harmless to health and  
the environment. The NO<sub>x</sub> performance of the three-way catalyst, however, rapidly  
30      deteriorates in the presence of oxygen.

Removal of NO<sub>x</sub> in lean-burn engines, *i.e.*, engines such as diesel engines that  
burn fuel in excess oxygen, continues to pose a great scientific challenge. There is

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sufficient motivation, however, to continue to pursue a practical solution for reducing NO<sub>x</sub> emissions in lean-burn engines because lean-burn engines provide better fuel economy than rich-burning engines. As previously mentioned, the NO<sub>x</sub> reducing performance of the three-way catalyst, which is the standard NO<sub>x</sub> abatement technology for gasoline engines, deteriorates rapidly in the presence of oxygen. Thus, this technology is ineffective in controlling NO<sub>x</sub> emissions in lean exhaust gases. Some of the approaches that have been considered in controlling NO<sub>x</sub> emissions in lean exhaust gases include catalytic decomposition of nitrogen monoxide (NO), selective catalytic reduction (SCR) with nitrogen containing compounds, and selective catalytic reduction with hydrocarbons (HC-SCR).

The decomposition of nitrogen monoxide to elements is described by the following equation:



The decomposition of nitrogen monoxide is thermodynamically favored under pressures and temperatures found in diesel exhaust. However, the decomposition reaction is inhibited by a high activation energy. Therefore, a catalyst is necessary to lower this activation energy in order to facilitate this decomposition. Various catalysts have been used to decompose NO, including precious metals, metallic oxides, and zeolites-based catalysts. One of the best catalysts recently suggested for NO decomposition is copper ion-exchanged zeolite ZSM5 (Cu/ZSM5). However, the catalytic activity of Cu/ZSM5 is greatly diminished in the presence of oxygen gas and sulfur dioxide, and the decomposition of NO is effective only at low space velocities.

In SCR with nitrogen containing compounds, a nitrogen compound, *e.g.*, ammonia or urea, is used as a reducing agent for nitrogen oxides to produce innocuous products. In reactions (2) and (3) below, ammonia is used as the reducing agent for nitrogen oxides to produce nitrogen and water:



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The reactions (2) and (3) are favored in the presence of oxygen. In the presence of oxygen, a catalyst such as vanadium pentoxide ( $V_2O_5$ ) supported on oxides such as  $TiO_2$ ,  $Al_2O_3$ , and  $SiO_2$  is used to facilitate the reaction. In  $NH_3$ -SCR, an external source of ammonia is needed to reduce  $NO_x$  to  $N_2$ .  $NH_3$ -SCR is widely used as a pollution reduction technique in stationary plants such as electric power plants. The toxicity and handling problems associated with ammonia, however, has limited the use of the technology in motor vehicles.

U.S. Patent 5,863,508 issued to Lachman *et al.* describes a multi-stage catalytic reactor system which allows ammonia to be synthesized onboard a vehicle and then used to reduce  $NO_x$  to  $N_2$  as previously described in reactions (2) and (3) above. The reactor system includes two units, each of which includes multiple open-ended cells. A portion of the cells in the first unit include a first stage catalyst, which is a noble metal on a support. The noble metal cannot be rhodium. Exhaust gases from combustion are passed through the first unit so that a portion of the  $NO_x$  in the exhaust gases is reduced to ammonia by the first stage catalyst. The modified exhaust gas mixture is then passed to the second unit, wherein the ammonia in the modified gas mixture is reacted with the remaining  $NO_x$  to yield a converted gas mixture. An external source of ammonia is not needed because the ammonia is generated in the first unit. The passage of the exhaust gases through the first and second units results in conversion of  $NO_x$ ,  $CO$ , and hydrocarbons to innocuous products. This technology is effective for lean burn engines.

HC-SCR was discovered during the survey of the effect of co-existing gases on the catalytic activity of Cu/ZSM5. In HC-SCR, hydrocarbons, *e.g.*, ethane, propane, and propene, selectively react with  $NO_x$  to produce nitrogen, carbon dioxide, and water:



There are three principal types of catalysts active for the HC-SCR, including zeolites, oxide-type catalysts, and supported noble metals. See, for example, Iwamoto, M. and Mizuno, N., "NO<sub>x</sub> emission control in oxygen-rich exhaust through selective catalytic reduction by hydrocarbon," Journal of Automobile Engineering (1993), pp. 23-33, and Fritz, A. and Pitchon, V., "The current state of research on automotive lean NO<sub>x</sub> catalysts," *supra*, pp. 10-25, for additional discussions on catalysts for HC-SCR. In this

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technology, additional HC must be supplied and a system is required to deliver the HC. Controlling the amount of HC needed is a great challenge. Furthermore, excess oxygen may affect NO<sub>x</sub> conversion.

#### SUMMARY OF THE INVENTION

5 In one aspect, the invention relates to a method for reducing NO<sub>x</sub> in lean exhaust gases to N<sub>2</sub>. The method comprises injecting a fuel into the exhaust gases and passing the exhaust gases and fuel mixture through a catalyst to reduce the NO<sub>x</sub> to N<sub>2</sub>.

10 In another aspect, the invention relates to a fuel injection system which comprises a catalytic reactor having an inlet end that receives exhaust gases and an outlet end that outputs converted exhaust gases. The fuel injection system further includes a catalyzed substrate mounted inside the catalytic reactor for reducing NO<sub>x</sub> in the received exhaust gases to N<sub>2</sub> in the presence of a fuel. The fuel injection system further includes a fuel injector for injecting the fuel upstream of the catalyzed substrate.

15 In another aspect, the invention relates to a catalyst composition for reducing NO<sub>x</sub> in lean exhaust gases to N<sub>2</sub> using a fuel as the reductant. In some embodiments, the catalyst composition comprises a perovskite compound represented by the formula AB<sub>1-x</sub>PM<sub>x</sub>O<sub>3</sub>, where A is a rare-earth metal, B is a transition metal, PM is a precious metal, and O is oxygen. In some embodiments, the catalyst composition comprises at least one metal oxide impregnated with at least one precious metal. In some 20 embodiments, the catalyst composition comprises a zeolite impregnated with at least one precious metal. In some embodiments, the catalyst composition comprises a combination of a zeolite and at least one metal oxide impregnated with at least one precious metal.

25 In another aspect, the invention relates to a catalytic unit for reducing NO<sub>x</sub> in lean exhaust gases to N<sub>2</sub> using a fuel as the reductant. In some embodiments, the catalytic unit comprises a body extruded from a zeolite which is impregnated with at least one precious metal. In some embodiments, the catalytic unit comprises a ceramic substrate coated with a catalytic material. In some embodiments, the catalytic material includes at least one metal oxide impregnated with at least one precious metal. In some 30 embodiments, the catalytic material includes a combination of a zeolite and at least one metal oxide impregnated with at least one precious metal. In some embodiments, the

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catalytic includes a perovskite compound represented by the formula  $AB_{1-x}PM_xO_3$ , where A is a rare-earth metal, B is a transition metal, PM is a precious metal, and O is oxygen.

5 Other aspects and advantages of the invention will be apparent from the following description and the appended claims.

#### BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1 schematically shows a reductant injection system in accordance with an embodiment of the invention.

10 Figure 2 shows a setup for evaluating the de $NO_x$  catalysts of the present invention.

#### DETAILED DESCRIPTION OF THE INVENTION

15 Embodiments of the invention provide a  $NO_x$  de-pollution (de $NO_x$ ) catalyst and a reductant injection system which uses the de $NO_x$  catalyst. In the reductant injection system, diesel fuel is post-injected into diesel exhaust gas and used as a reductant for the reduction of  $NO_x$  to  $N_2$  through the de $NO_x$  catalyst. Diesel fuel is injected continuously or periodically based on the requirement of the total  $NO_x$  conversion and fuel penalty. In some embodiments of the invention, the de $NO_x$  catalyst includes one or more perovskite compounds represented by the formula  $AB_{1-x}PM_xO_3$ , where A is a group III or group IV rare-earth metal, B is a group III or group IV transition metal, PM is a precious metal, O is oxygen. Preferably, x ranges from 0.01 to 0.3. In some embodiments of the invention, the de $NO_x$  catalyst includes a support material impregnated with a precious metal or a combination of precious metals. The support material is made of a metal oxide or a combination of two or more metal oxides. In some embodiments of the invention, the de $NO_x$  catalyst includes a zeolite impregnated 20 with a precious metal, or a combination of precious metals. Zeolites are silicates consisting of interlocking tetrahedrons of  $SiO_4$  and  $AlO_4$ . In some embodiments, of the invention, the de $NO_x$  catalyst includes a combination of a zeolite and metal oxide 25 impregnated with a precious metal, or a combination of precious metals.

30 Various embodiments of the invention will now be described with reference to the accompanying figures. Figure 1 schematically shows a reductant injection system 2

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which includes a catalytic reactor 4 having an inlet end 6 for receiving exhaust gases 8 and an outlet end 10 for outputting converted exhaust gases 12. A deNO<sub>x</sub> catalyst 14 is mounted inside the catalytic reactor 4. A port 16 is provided in the wall of the catalytic reactor 4, upstream of the deNO<sub>x</sub> catalyst 14. The reductant injection system 2 further comprises a fuel injector 18 which is coupled to the port 16. Preferably, the fuel injector 18 is as close as possible to the deNO<sub>x</sub> catalyst 14. In operation, exhaust gases 8 are introduced into the catalytic reactor 4 through the inlet end 6. Diesel fuel 20 is injected into the catalytic reactor 4 through the port 16. The diesel fuel 20 may be injected continuously or periodically. The injected diesel fuel 20 mixes with the exhaust gases 8. The resulting mixture then passes through the deNO<sub>x</sub> catalyst 14. The deNO<sub>x</sub> catalyst 14 converts NO<sub>x</sub> into innocuous products. The converted gas mixture 12 exits the catalytic reactor 4 through the outlet end 10.

Catalytic activities of various embodiments of the deNO<sub>x</sub> catalyst 14 are evaluated by placing individual deNO<sub>x</sub> catalysts inside the catalytic reactor 4 and passing exhaust gases mixed with diesel fuel through the catalysts. For the reduction of NO<sub>x</sub> to N<sub>2</sub> using diesel fuel, simulated diesel exhaust gases having the composition indicated in Table 1 are introduced into the inlet end 6 of the catalytic reactor 4.

Table 1: Composition of Simulated Diesel Exhaust Gases

Gas	Amount (by volume)
O <sub>2</sub>	3-6 percent
CO <sub>2</sub>	14 percent
NO <sub>x</sub>	500-1065 ppm
CO	350 ppm
H <sub>2</sub> O	10-12 percent

The conversion of NO<sub>x</sub> to N<sub>2</sub> is studied by varying the amount of diesel fuel injected through the port 16 into the catalytic reactor 2. In the study, the diesel fuel is injected by a gasoline fuel injector, which, for safety reasons, had a lower pressure in comparison with a typical diesel fuel injector. This lower injection pressure may result

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in incomplete fuel consumption. The typical fuel injection rates in the study are 2.2 mg/s, 1.75 mg/s, and 1.4 mg/s of diesel fuel, which correspond to 0.004, 0.0035, and 0.003 injection cycles, respectively. In a period of  $t$  seconds,  $u$  injection cycle means that the fuel is injected for  $t*u$  seconds. For a 1000-second period, for example, 0.004 injection cycle means that the fuel is injected for 4 seconds.

5 For comparison purposes, catalyst activity using synthetic hydrocarbons as the exhaust gases is also investigated. For the reduction of  $\text{NO}_x$  to  $\text{N}_2$  using synthetic hydrocarbons, synthetic gas mixture having the composition indicated in Table 2 is introduced into the inlet end 6 of the catalytic reactor 4.

10

Table 2: Composition of Synthetic Gas Mixture

Gas	Amount (by volume)
$\text{O}_2$	0.77 percent
$\text{CO}_2$	14 percent
$\text{NO}_x$	1000 ppm
CO	1000 ppm
$\text{C}_3\text{H}_6$	333 ppm
$\text{C}_3\text{H}_8$	167 ppm
$\text{H}_2$	0.33 percent
$\text{H}_2\text{O}$	10-12 percent

15

The synthetic gas mixture in Table 2 gives approximately 1.2 redox ratio. The synthetic gas flow is nitrogen-balanced, resulting in a total flow of 7508 ml/min. This flow rate corresponds to a space velocity of 35,000 per hour. The space velocity can be varied by adjusting the feed flow rates of the gas mixture. Typically, the catalytic activity is measured with the catalytic reactor 2 operating within a temperature range of 60 °C to 600 °C. A temperature ramp rate is set for 8.5 °C/min until the catalytic reactor 2 reaches 600 °C, and then the operating temperature of the catalytic reactor 2 is maintained at this temperature for approximately 15 minutes.

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Prior to each run, the gases introduced into the inlet end 6 of the catalytic reactor 2 are quantified. A mass balance of the initial  $\text{NO}_x$  concentration in the inlet gas mixture with respect to the amount of  $\text{NH}_3$ ,  $\text{N}_2\text{O}$ , and  $\text{NO}_2$  formed downstream of the catalyzed substrate is used to determine the amount of  $\text{N}_2$  produced. The percent 5 total NO conversion and the percent amount of  $\text{NH}_3$  and  $\text{N}_2$  formed are determined by the following equations:

$$\text{Total NO conversion}(\%) = \left[ \left( \frac{C_{\text{NO}}}{C_{\text{NO,in}}} \right) - 1 \right] \times 100 \quad (5)$$

$$\text{NH}_3(\%) = \frac{C_{\text{NH}_3}}{C_{\text{NO,in}}} \times 100 \quad (6)$$

$$\text{N}_2(\%) = \text{NO conversion}(\%) - [\text{NH}_3(\%) + \text{NO}_2(\%) + 2 \times \text{N}_2\text{O}(\%)] \quad (7)$$

As shown in Figure 2, the converted gas mixture 12 downstream of the  $\text{deNO}_x$  catalyst 14 is analyzed by a Fourier Transform Infrared Spectrometer (FTIR) 22, such as one sold under the trade name Magna Infrared 560 Spectrometer by Nicolet Instrument 10 Corporation, Madison, WI. FTIR 22 allows all the species of interest such as  $\text{NO}$ ,  $\text{NH}_3$ ,  $\text{N}_2\text{O}$ ,  $\text{NO}_2$ ,  $\text{CO}$ ,  $\text{CO}_2$ ,  $\text{H}_2\text{O}$ ,  $\text{C}_3\text{H}_6$ ,  $\text{C}_3\text{H}_8$ , and other hydrocarbons to be simultaneously monitored.

The following examples of  $\text{deNO}_x$  catalysts are subjected to the testing 15 procedure to determine their effectiveness in converting  $\text{NO}_x$  to innocuous products using the reductant injection system 2 described above. It should be clear that the following examples are intended for illustration purposes and are not intended to limit the scope of the invention as otherwise described herein.

#### EXAMPLE 1

In one embodiment of the invention, the  $\text{deNO}_x$  catalyst 14 (shown in Figure 1) 20 includes one or more perovskite compounds represented by the formula  $\text{AB}_{1-x}\text{PM}_x\text{O}_3$ , where A is a group III or group IV rare-earth metal, B is a group III or group IV transition metal, PM is a precious metal, O is oxygen. Preferably, x ranges from 0.01

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to 0.3. To obtain a relatively high surface area, the perovskite-based deNO<sub>x</sub> catalyst can be synthesized by a method called the Pechini process. For a C1 deNO<sub>x</sub> catalyst based on a perovskite compound LaMn<sub>0.9</sub>Ru<sub>0.1</sub>O<sub>3</sub>, the Pechini process involves dissolving lanthanum nitrate in aqueous manganese nitrate and adding citric acid and ethylene glycol to the mixture to obtain a chelated complex. The ratio of citric acid to lanthanum (La) and manganese (Mn) is one to one, *e.g.*, two moles of citric acid to one mole of LaMn<sub>0.9</sub>Ru<sub>0.1</sub>O<sub>3</sub>. The amount of ethylene glycol to add to the mixture is calculated by the following equation:

$$\frac{\text{weight of ethylene glycol}}{\text{density of ethylene glycol}} = 1.5 \times \frac{\text{weight of citric acid}}{x} \quad (8)$$

The chelated complex is heated to 90 °C to form a gel. The temperature of the gel is then increased to 120 °C to remove all the water and NO<sub>x</sub> fumes, and the gel is puffed out, *i.e.*, ignited, to get the powder. The puffed-out powder is fired at 450 °C for 4 hours to dry and remove carbon from the powder. After that, the powder is sintered at 700 °C or any desirable temperature to get the final product. The powder is ball milled for 2-5 days. About 90 percent of the milled powder is then combined with about 10 percent of a binder, *e.g.*, colloidal alumina sold under the trade name Al-20 by PQ corporation, Philadelphia, PA, to form a washcoat slurry. A ceramic substrate, *e.g.*, cordierite honeycombs made by Corning, Inc., Corning, New York, under the trade name Celcor®, is dipped in the washcoat slurry. In general, any ceramic substrate that can withstand temperatures of about 150 °C to 600 °C can be used in the invention. The ceramic substrate is fired in air or reducing atmosphere, *e.g.*, forming gas or nitrogen gas, or exhaust gas at 600 °C for 3 hours with a ramp rate of 3 °C/min.

The composition of the C1 deNO<sub>x</sub> catalyst is as follows: 90 percent LaMn<sub>0.9</sub>Ru<sub>0.1</sub>O<sub>3</sub> and 10 percent Al<sub>2</sub>O<sub>3</sub>. Activity of this catalyst in simulated diesel exhaust gases (see Table 1) was evaluated using the testing procedure outlined above (see Figure 2). As shown in Table 3, the C1 deNO<sub>x</sub> catalyst demonstrated a high total NO conversion of 81.5 to 96.3 percent with diesel fuel injection rate of 1.4 mg/s and outlet temperature of 300 °C to 500 °C, *i.e.*, temperature at the outlet end 10 of the catalytic reactor 2 (shown in Figure 1). About 70 to 84 percent of N<sub>2</sub> is generated in the outlet temperature window with 10 to 12 percent NH<sub>3</sub> as a by-product. The

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concentrations of  $N_2O$  and  $NO_2$  are negligible. The high NO conversion indicates that C1 can crack the diesel fuel efficiently to lighter hydrocarbon or reducing agents which can enhance the reduction of  $NO_x$  to  $N_2$ . Decreasing the amount of the diesel fuel injected upstream of the catalyst can reduce the amount of  $NH_3$  produced.

5 Table 3: Summary of Catalyst Activity for C1 De $NO_x$  Catalyst Using Simulated Diesel Exhaust Gases

O <sub>2</sub> (%)	Diesel Injection Rate (mg/s)	Outlet Temp. (°C)	Total NO Conversion (%)	NH <sub>3</sub> (%)	N <sub>2</sub> (%)	Initial NO (ppm)
6	1.4	300	88.5	11.5	77	480
6	1.4	350	92.3	10.4	81.9	480
6	1.4	380	95.9	12.5	83.4	480
6	1.4	404	96.3	11.7	84.6	480
6	1.4	430	95.4	11.0	84.4	480
6	1.4	483	79.4	10.4	69	480
6	1.4	520	81.5	11.5	70	480

10 For comparison purposes, the catalytic performance of the C1 de $NO_x$  catalyst was also tested in a synthetic gas mixture (see Table 2). In this case, the synthetic gases were used as reductants. As shown in Table 4, the highest NO to N<sub>2</sub> conversion observed is 33.5 percent at outlet temperature of 576 °C. At lower temperatures such as 300 °C, NO conversion was as low as 4 percent. As can be observed from the data in Tables 3 and 4, the NO to N<sub>2</sub> conversion is much lower when synthetic gases were used instead of diesel fuel.

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Table 4: Summary of Catalyst Activity for C1 DeNO<sub>x</sub> Catalyst Using Synthetic Gas

## Mixture

O <sub>2</sub> (%)	Diesel Injection Rate (mg/s)	Outlet Temp. (°C)	Total NO Conversion (%)	NH <sub>3</sub> (%)	N <sub>2</sub> (%)	Initial NO (ppm)
6	0	300	4	0	4	1080
6	0	400	12	0	12	1080
6	0	500	25.5	0	25.5	1080
6	0	576	33.5	0	33.5	1080

EXAMPLE 2

5        In another embodiment of the invention, the deNO<sub>x</sub> catalyst 14 includes a support material impregnated with one or more precious metals. Examples of precious metals suitable for use in the invention are rhodium (Rh), platinum (Pt), palladium (Pd), iridium (Ir), and ruthenium (Ru). The support material is made of a metal oxide or a combination of two or more metal oxides. A C2 deNO<sub>x</sub> catalyst is attained by 10 impregnation of non-stoichiometric titanium oxide (TiO<sub>2-x</sub>) with Rh and Pt. In this example, x is 0.25. The non-stoichiometric titanium oxide is obtained by mixing one mole of Ti<sub>2</sub>O<sub>3</sub> and two moles of TiO<sub>2</sub> and then firing the mixture at 1100 °C for 5 hours in forming gas (6 percent H<sub>2</sub>/94 percent N<sub>2</sub>). The fired mixture is impregnated with Pt by dipping repeatedly in (NH<sub>3</sub>)<sub>4</sub>Pt(NO<sub>3</sub>)<sub>2</sub> solution. The resulting mixture is dried in an oven at 110 °C to 120 °C for 24 hours and then fired for three hours in air at 560°C. 15        The Pt-TiO<sub>2-x</sub> mixture is impregnated with Rh by dipping repeatedly in Rh solution. The resulting mixture is dried in an oven at 110 °C to 120 °C for 24 hours and then fired for three hours in air at 560°C to obtain Rh-Pt/TiO<sub>2-x</sub>.

20        The fired mixture Rh-Pt/TiO<sub>2-x</sub> is milled for 2-5 days. Then about 90 percent of the milled powder is combined with about 10 percent of a binder, e.g., colloidal alumina, to form a washcoat slurry. A ceramic substrate, e.g., cordierite honeycombs sold by Corning, Inc., Corning, NY, under the trade name Celcor®, is dipped or

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washcoated in the slurry. In general, any ceramic substrate that can withstand temperatures of approximately 150 °C to 600 °C can be used in the invention. A washcoat loading in the range of 30 to 40 percent is observed on the honeycomb substrate. The washcoated substrate is then fired in air or reducing atmosphere, *e.g.*, forming gas or nitrogen gas, or exhaust gas at 600 °C for 3 hours with ramp rate of 3 °C/min. The composition of the C2 deNO<sub>x</sub> catalyst is as follows: 1 percent by weight Rh, 2 percent by weight Pt, 90 percent by weight TiO<sub>2-x</sub>, and 10 percent by weight Al<sub>2</sub>O<sub>3</sub> (binder). Typically, the amount of Rh will be in a range from 0.01 to 5 percent, the amount of Pt will be in a range from 0.01 to 5 percent, and the amount of TiO<sub>2-x</sub> will be in a range from 0 to 100%.

Activity of the C2 deNO<sub>x</sub> catalyst in simulated diesel exhaust gases (see Table 1) was evaluated using the testing procedure described above (see Figure 2). As shown in Table 5, the C2 deNO<sub>x</sub> catalyst demonstrated a high total NO conversion of 73 to 81.6 percent with diesel fuel injection rate of 1.75 mg/s and catalytic reactor outlet temperature of 450 °C to 560 °C. For a diesel injection rate of 2.2 mg/s and catalytic reactor outlet temperature of 445 °C to 562 °C, the C2 deNO<sub>x</sub> catalyst demonstrated a very high total NO conversion of 91.8 to 96.4 percent. This shows that increasing the fuel injection amount results in higher N<sub>2</sub> generation. However, the undesirable NH<sub>3</sub> generation also increases as the fuel injection amount is increased (see Table 5). For the C2 deNO<sub>x</sub> catalyst, the optimized condition is that the injection amount is less than 1.75 mg/s.

Table 5: Summary of Catalyst Activity for C2 DeNO<sub>x</sub> Catalyst Using Simulated Diesel Exhaust Gases

O <sub>2</sub> (%)	Diesel Injection Rate (mg/s)	Outlet Temp. (°C)	Total NO Conversion (%)	NH <sub>3</sub> (%)	N <sub>2</sub> (%)	Initial NO (ppm)
6	1.75	450	73	4	69	511
6	1.75	480	77.1	4.1	73	511
6	1.75	520	81.6	6.1	75.5	511
6	1.75	560	76.7	6.8	70	511
6	2.2	445	91.8	11.2	80.6	501
6	2.2	490	96.4	11.6	84.8	501
6	2.2	518	94.6	12.6	82	501
6	2.2	562	93	10.4	82.6	501

EXAMPLE 3

5           In another embodiment of the invention, the deNO<sub>x</sub> catalyst 14 (shown in Figure 1) includes a zeolite impregnated with one or more precious metals. Examples of precious metals suitable for use in the invention are Pt, Rh, Ru, Pd, and Ir. As previously mentioned, zeolites are silicates consisting of interlocking tetrahedrons of SiO<sub>x</sub> and AlO<sub>y</sub>. An example of a zeolite that is suitable for use in the invention is 10 ZSM-5. For high temperature stability, the silica to alumina mole ratio in the zeolite should be high. For example, for ZSM-5, the silica to alumina mole ratios is at least about 25, and preferably at least about 55. One source of ZSM-5 zeolite is supplied by Exxon Mobil Corp., Dallas, TX, under the trade name MZ-12. Other examples of zeolites evaluated for use in the invention include mesoporous crystalline material 15 (MCM-41), ultrastabilized Y (USY), NaY, H-ferrierite, and AlPO<sub>4</sub>-5. In some embodiments of the invention, the zeolites are loaded with transition metals, e.g., Cu, In, Ga, Ni, Ag, or Co, or combinations thereof. H-ferrierite loaded with Ni-Co or Ag

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has been shown to be effective in reducing NO<sub>2</sub> to N<sub>2</sub>. The catalyst may include up to 5 percent precious metals and up to 5 percent transition metals.

A C3 deNO<sub>x</sub> catalyst is attained by impregnation of Ni-Co loaded MZ-12 (ZSM-5; Si/Al=55) zeolite with Pt. MZ-12 zeolite is loaded with 1.5 percent Ni and 1.5 percent Co. The metals, Ni and Co, are added as their nitrate precursors. The MZ-12 zeolite is first weighed out, and amounts of nickel nitrate and cobalt nitrate to be combined with the zeolite are calculated. The nitrates are then dissolved in deionized water. MZ-12 zeolite powder is dispersed in the solution. The mixture is then stirred well followed by drying in an oven at about 110 °C to 120 °C for about 24 hours. The resulting dried powder is calcined at a ramp rate of 3 °C/min to about 600 °C and held at that temperature for about 3 hours in air to obtain Ni-Co/MZ-12. The calcined mixture is extruded into honeycombs. Prior to extrusion, specific amounts of methocel, silicon resin, dibenzyl ether, and oleic acid are added to the calcined mixture. Both 200 and 400 cell density per square inch (cpsi) were extruded and fired at 850 °C for 3 hours. The extruded honeycomb bodies were impregnated with 2 percent Pt by dipping repeatedly in a 2 percent (NH<sub>3</sub>)<sub>4</sub>Pt(NO<sub>3</sub>)<sub>2</sub> solution. Prior to catalytic testing, the samples are fired under air for 3 hours at 600 °C.

The composition of the C3 deNO<sub>x</sub> catalyst is as follows: 2 percent Pt, 1.5 percent Ni, 1.5 percent Co, 90 percent MZ-12, and 10 percent Al<sub>2</sub>O<sub>3</sub>. Activity of this catalyst in simulated diesel exhaust gases (see Table 1) was evaluated using the testing procedure outlined above. As shown in Table 6, the C3 deNO<sub>x</sub> catalyst demonstrated a high total NO conversion of 71 to 77 percent with diesel fuel injection rate of 1.4 mg/s and catalytic reactor outlet temperature of 446 °C to 505 °C. For a diesel injection rate of 2.2 mg/s and catalytic reactor outlet temperature of 550 °C to 600 °C, the C3 deNO<sub>x</sub> catalyst demonstrated a high total NO conversion of 86 percent.

Table 6: Summary of Catalyst Activity for C3 DeNO<sub>x</sub> Catalyst Using Simulated Diesel Exhaust Gases

O <sub>2</sub> (%)	Diesel Injection Rate (mg/s)	Outlet Temp. (°C)	Total NO Conversion (%)	NH <sub>3</sub> (%)	N <sub>2</sub> (%)	Initial NO (ppm)
3	1.4	446	71.2	7	64.2	1065
3	1.4	505	77	7.5	69.5	1065
6	2.2	550-600	86.1	9	77.1	524

EXAMPLE 4

5        In another embodiment of the invention, the deNO<sub>x</sub> catalyst 14 (shown in Figure 1) includes a zeolite and metal-oxide mixture impregnated with one or more precious metals. A C4 deNO<sub>x</sub> catalyst is attained by impregnation of 50 percent MZ-12 (ZSM-5; Si/Al=55) zeolite and alumina mixture with a 1.12 g iridium (Ir) solution made from IrCl<sub>3</sub>·3H<sub>2</sub>O to achieve a 45 g/ft<sup>3</sup> washcoat loading on a 3.25 in. x 1 in. ceramic substrate, *e.g.*, cordierite honeycombs made by Corning, Inc., Corning, NY, under the trade name Celcor®, with a cell density of 400 cpsi. The alumina in the zeolite and alumina mixture may exist in its various forms including La- $\gamma$ - $\beta$ -Al<sub>2</sub>O<sub>3</sub>. The C4 catalyst is prepared using a method similar to the one described for the C2 catalyst. The alumina binder used in this example is 15 percent colloidal alumina, *e.g.*, colloidal alumina under the trade name Al-20 by PQ corporation. All catalytically tested substrates have a diameter of about 1 inch and a length of about 1 inch. In an alternative embodiment, the C4 deNO<sub>x</sub> catalyst may be formed by drying the zeolite, alumina, and iridium mixture in an oven and then firing the dried mixture. The fired mixture may be extruded into honeycombs.

10      15      20      The composition of the C4 deNO<sub>x</sub> catalyst is as follows: 1 percent Ir, 50 percent ZSM-5 zeolite, such as one sold under the trade name MZ-12 by Exxon Mobil, Corp., Dallas, TX, and 50 percent Al<sub>2</sub>O<sub>3</sub>. Activity of this catalyst in simulated diesel exhaust gases (see Table 1) was evaluated using the testing procedure outlined above. The

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catalytic activity was evaluated under various oxygen concentrations (3 to 5 percent) with constant fuel injection rate of 1.4 mg/s. As shown in Table 7, the C4 deNO<sub>x</sub> catalyst demonstrated a high total NO conversion of 70 to 96 percent with diesel fuel injection rate of 1.4 mg/s and catalytic reactor outlet temperature of 390 °C to 516 °C. 5 Maximum N<sub>2</sub> generations of 93 percent, 90.7 percent, and 83.4 percent were observed at 400 °C with 3 percent, 4 percent, and 5 percent oxygen, respectively. The N<sub>2</sub> generation decreased with increasing temperature. The undesirable by-product NH<sub>3</sub> was relatively low. The total NO<sub>x</sub> conversion using catalyst C4 were very high when the simulated diesel exhaust gases contained 3 percent and 4 percent oxygen.

10 Table 7: Summary of Catalyst Activity for C4 DeNO<sub>x</sub> Catalyst Using Simulated Diesel Exhaust Gases

O <sub>2</sub> (%)	Diesel Injection Rate (mg/s)	Outlet Temp. (°C)	Total NO Conversion (%)	NH <sub>3</sub> (%)	N <sub>2</sub> (%)	Initial NO (ppm)
3	1.4	400	96	3	93	525
3	1.4	419	96.6	11.6	85	525
4	1.4	390	94.1	3.4	90.7	525
4	1.4	431	95.4	6.3	89.1	525
5	1.4	393	87.4	4	83.4	525
5	1.4	438	62.7	3	59.7	525
5	1.4	516	70.5	4.6	65.9	525

The deNO<sub>x</sub> catalysts of the invention demonstrate high activities for the reduction of NO<sub>x</sub> to N<sub>2</sub> in simulated diesel exhaust gases using diesel fuel as reductant. 15 No other fuel or gas tanks are needed to be installed because on-board diesel fuel can be used. The amounts of NO<sub>2</sub> and N<sub>2</sub>O generation are minimal. The catalyst may be extruded, resulting in a material with a larger volume of catalyst than in the washcoated case, which may lead to enhanced performance. It is observed by FTIR (22 in Figure 2) that a lot of light hydrocarbons are not used, which means that fuel penalty can be decreased. A partial oxidation catalyst (not shown) may be added downstream of the 20

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deNO<sub>x</sub> catalysts (14 in Figure 1). Adding a partial oxidation catalyst downstream of the deNO<sub>x</sub> catalysts can (a) decrease the emission of the hydrocarbon into atmosphere, (b) use the hydrocarbon generated by diesel fuel partial oxidation to reduce NO to N<sub>2</sub>, (subsequently, NO is also reduced by acting as an oxidant for the hydrocarbon) and (c) 5 decrease the requirement of the NO conversion at the deNO<sub>x</sub> catalyst, *i.e.*, the amount of the fuel injected will be decreased.

To enhance total NO<sub>x</sub> reduction, some metal or metal oxides are active for partially cracking diesel into lighter and efficient reductants. Such metal or metal oxides may include the following: precious metal, transition metal/metal oxide, and 10 rare earth metal/metal oxide or their combination. A considerable advantage in activity is expected to be gained from a high pressure diesel injector, which will atomize the fuel. Perovskite compound has low surface area. Its catalytic performance can be enhanced by increasing surface area with different synthesizing methods, *e.g.*, the 15 Pechini process described above. Gasoline is an alternative reductant that may be used instead of diesel to reduce charring. Gasoline is expected to lower the light off temperature for NO<sub>x</sub> reduction.

While the invention has been described with respect to a limited number of 20 embodiments, those skilled in the art, having benefit of this disclosure, will appreciate that other embodiments can be devised which do not depart from the scope of the invention as disclosed herein. Accordingly, the scope of the invention should be limited only by the attached claims.

CLAIMS

What is claimed is:

1. A method for reducing NO<sub>x</sub> in lean exhaust gases to N<sub>2</sub>, the method comprising:
  - 5 injecting a fuel into the exhaust gases; and
  - passing the exhaust gases and fuel mixture through a catalyst to reduce the NO<sub>x</sub> in the exhaust gases to N<sub>2</sub>.
2. The method of claim 1, further comprising passing the NO<sub>x</sub> reduced exhaust
  - 10 gases through a partial oxidation catalyst.
3. The method of claim 1, wherein the fuel is selected from the group consisting of diesel fuel and gasoline.
- 15 4. The method of claim 1, wherein the catalyst comprises a perovskite compound represented by the formula AB<sub>1-x</sub>PM<sub>x</sub>O<sub>3</sub>, where A is a rare-earth metal, B is a transition metal, PM is a precious metal, and O is oxygen.
5. The method of claim 4, wherein A comprises lanthanum, B comprises manganese,
  - 20 PM comprises ruthenium, and x ranges from about 0.01 to 0.3.
6. The method of claim 1, wherein the catalyst comprises at least one metal oxide impregnated with at least one precious metal.
- 25 7. The method of claim 6, wherein the metal oxide comprises one selected from the group consisting of TiO<sub>2-x</sub> and Al<sub>2</sub>O<sub>3</sub>.
8. The method of claim 7, wherein x is 0.25.
- 30 9. The method of claim 6, wherein the precious metal is selected from the group consisting of Pt, Pd, Rh, Ru, Ir, and combinations thereof.

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10. The method of claim 1, wherein the catalyst comprises a zeolite impregnated with at least one precious metal.
- 5 11. The method of claim 10, wherein the zeolite comprises one selected from the group consisting of MCM-41, ultrastabilized Y, NaY, H-ferrierite, AlPO<sub>4</sub>-5, and ZSM-5.
- 10 12. The method of claim 8, wherein the zeolite is loaded with a metal selected from the group consisting of Cu, Ni, In, Ga, Ag, Co, and combinations thereof.
- 15 13. The method of claim 1, wherein the catalyst comprises a combination of a zeolite and at least one metal oxide impregnated with at least one precious metal.
14. The method of claim 13, wherein the metal oxide comprises Al<sub>2</sub>O<sub>3</sub>.
- 15 15. The method of claim 13, wherein the precious metal comprises one selected from the group consisting of Pt, Pd, Rh, Ru, Ir, and combinations thereof.
- 20 16. The method of claim 13, wherein the zeolite comprises one selected from the group consisting of MCM-41, ultrastabilized Y, NaY, H-ferrierite, AlPO<sub>4</sub>-5, and ZSM-5.
- 25 17. An exhaust gas NO<sub>x</sub> reducing system, comprising:
  - a catalytic reactor having an inlet end which receives the exhaust gases and an outlet end which outputs converted exhaust gases;
  - a catalyzed substrate mounted inside the catalytic reactor for reducing NO<sub>x</sub> in the received exhaust gases to N<sub>2</sub> in the presence of a fuel; and
  - a fuel injector for injecting the fuel upstream of the catalyzed substrate.
- 30 18. The system of claim 17, further comprising a partial oxidation catalyst mounted downstream of the catalyzed substrate.

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19. The system of claim 17, wherein the fuel comprises one selected from a group consisting of diesel fuel and gasoline.
- 5 20. The system of claim 17, wherein the catalyst comprises a perovskite compound represented by the formula  $AB_{1-x}PM_xO_3$ , where A is a rare-earth metal, B is a transition metal, PM is a precious metal, and O is oxygen.
- 10 21. The system of claim 20, wherein A comprises lanthanum, B comprises manganese, PM comprises ruthenium, and x ranges from about 0.01 to 0.3.
- 15 22. The system of claim 17, wherein the catalyst comprises at least one metal oxide impregnated with at least one precious metal.
23. The system of claim 22, wherein the metal oxide comprises  $TiO_{2-x}$ .
24. The system of claim 22, wherein the precious metal comprises one selected from the group consisting of Pt, Pd, Rh, Ru, Ir, and combinations thereof.
- 25 25. The system of claim 17, wherein the catalyst comprises a zeolite impregnated with at least one precious metal.
26. The system of claim 25, wherein the zeolite comprises one selected from the group consisting of MCM-41, ultrastabilized Y, NaY, H-ferrierite, AlPO<sub>4</sub>-5, and ZSM-5.
- 25 27. The system of claim 25, wherein the zeolite is loaded with a metal selected from the group consisting of Cu, Ni, In, Ga, Ag, Co, and combinations thereof.
- 30 28. The system of claim 25, wherein the precious metal comprises one selected from the group consisting of Pt, Pd, Rh, Ru, Ir, and combinations thereof.

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29. The system of claim 17, wherein the catalyst comprises a combination of a zeolite and at least one metal oxide impregnated with at least one precious metal.

5 30. The system of claim 29, wherein the zeolite comprises one selected from the group consisting of MCM-41, ultrastabilized Y, NaY, H-ferrierite, AlPO<sub>4</sub>-5, and ZSM-5.

10 31. The system of claim 29, wherein the precious metal comprises one selected from the group consisting of Pt, Pd, Rh, Ru, Ir, and combinations thereof.

15 32. The system of claim 29, wherein the metal oxide comprises Al<sub>2</sub>O<sub>3</sub>.

33. A catalyst composition for reducing NO<sub>x</sub> in lean exhaust gases to N<sub>2</sub> using a fuel as a reductant, comprising a perovskite compound represented by the formula AB<sub>1-x</sub>PM<sub>x</sub>O<sub>3</sub>, where A is a rare-earth metal, B is a transition metal, PM is a precious metal, and O is oxygen.

20 34. The catalyst composition of claim 33, wherein x ranges from about 0.01 to 0.3.

35. The catalyst composition of claim 33, wherein A comprises lanthanum.

25 36. The catalyst composition of claim 33, wherein B comprises manganese.

37. The catalyst composition of claim 33, wherein PM comprises platinum.

38. The catalyst composition of claim 33, wherein A comprises lanthanum, B comprises manganese, PM comprises platinum, and x ranges from about 0.01 to 0.3.

30 39. A catalyst composition for reducing NO<sub>x</sub> in lean exhaust gases to N<sub>2</sub> using a fuel as the reductant, comprising at least one metal oxide impregnated with at least one precious metal.

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40. The catalyst composition of claim 39, wherein the metal oxide comprises  $TiO_{2-x}$ .

41. The catalyst composition of claim 39, wherein the precious metal comprises one selected from the group consisting of Rh, Pt, Pd, Ir, Ru, and combinations thereof. 5

42. A catalyst composition for reducing  $NO_x$  in lean exhaust gases to  $N_2$  using a fuel as a reductant, comprising a zeolite impregnated with at least one precious metal.

10 43. The catalyst composition of claim 42, wherein the zeolite comprises one selected from the group consisting of MCM-41, ultrastabilized Y, NaY, AlPO<sub>4</sub>-5, H-ferrierite, and ZSM-5.

15 44. The catalyst composition of claim 42, wherein the zeolite is loaded with a metal selected from the group consisting of Cu, Ni, In, Ga, Ag, Co, and combinations thereof.

45. The catalyst composition of claim 42, wherein the precious metal comprises one selected from the group consisting of Pt, Pd, Rh, Ru, Ir, and combinations thereof.

20 46. A catalyst composition for reducing  $NO_x$  in lean exhaust gases to  $N_2$  using a fuel as a reductant, comprising a combination of a zeolite and at least one metal oxide impregnated with at least one precious metal.

25 47. The catalytic composition of claim 46, wherein the zeolite comprises one selected from the group consisting of MCM-41, ultrastabilized Y, NaY, H-ferrierite, AlPO<sub>4</sub>-5, and ZSM-5.

48. The catalytic composition of claim 47, wherein the precious metal comprises one selected from the group consisting of Pt, Pd, Rh, Ru, Ir, and combinations thereof.

30 49. The catalytic composition of claim 47, wherein the metal oxide comprises  $Al_2O_3$ .

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50. A catalytic unit for reducing NO<sub>x</sub> in lean exhaust gases to N<sub>2</sub> using a fuel as a reductant, comprising a body extruded from a zeolite which is impregnated with at least one precious metal.

5 51. The catalyst unit of claim 50, wherein the zeolite comprises one selected from the group consisting of MCM-41, ultrastabilized Y, NaY, H-ferrierite, AlPO<sub>4</sub>-5, and ZSM-5.

10 52. The catalyst unit of claim 50, wherein the zeolite is loaded with a metal selected from the group consisting of Cu, Ni, In, Ga, Ag, Co, and combinations thereof.

15 53. The catalytic unit of claim 50, wherein the precious metal comprises one selected from the group consisting of Pt, Pd, Rh, Ru, Ir, and combinations thereof.

20 54. A catalytic unit for reducing NO<sub>x</sub> in exhaust gases to N<sub>2</sub> using a fuel as a reductant, comprising a ceramic substrate coated with at least one metal oxide impregnated with at least one precious metal.

55. The catalytic unit of claim 54, wherein the metal oxide comprises TiO<sub>2-x</sub>.

25 56. The catalytic unit of claim 54, wherein the precious metal comprises one selected from the group consisting of Pt, Pd, Rh, Ru, Ir, and combinations thereof.

57. A catalytic unit for reducing NO<sub>x</sub> in exhaust gases to N<sub>2</sub> using a fuel as a reductant, comprising a ceramic substrate coated with a perovskite compound represented by the formula AB<sub>1-x</sub>PM<sub>x</sub>O<sub>3</sub>, where A is a rare-earth metal, B is a transition metal, PM is a precious metal, and O is oxygen.

30 58. The catalyst unit of claim 57, wherein A comprises lanthanum, B comprises manganese, PM comprises platinum, and x ranges from about 0.01 to 0.3.

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59. A catalytic unit for reducing  $\text{NO}_x$  in exhaust gases to  $\text{N}_2$  using a fuel as a reductant, comprising a ceramic substrate coated with a combination of a zeolite and at least one metal oxide impregnated with at least one precious metal.

5 60. The catalytic unit of claim 59, wherein the zeolite comprises one selected from the group consisting of MCM-41, ultrastabilized Y, NaY, H-ferrierite,  $\text{AlPO}_4\text{-5}$ , and ZSM-5.

10 61. The catalytic unit of claim 59, wherein the precious metal comprises one selected from the group consisting of Pt, Pd, Rh, Ru, Ir, and combinations thereof.

62. The catalytic unit of claim 59, wherein the metal oxide comprises  $\text{Al}_2\text{O}_3$ .

1/1

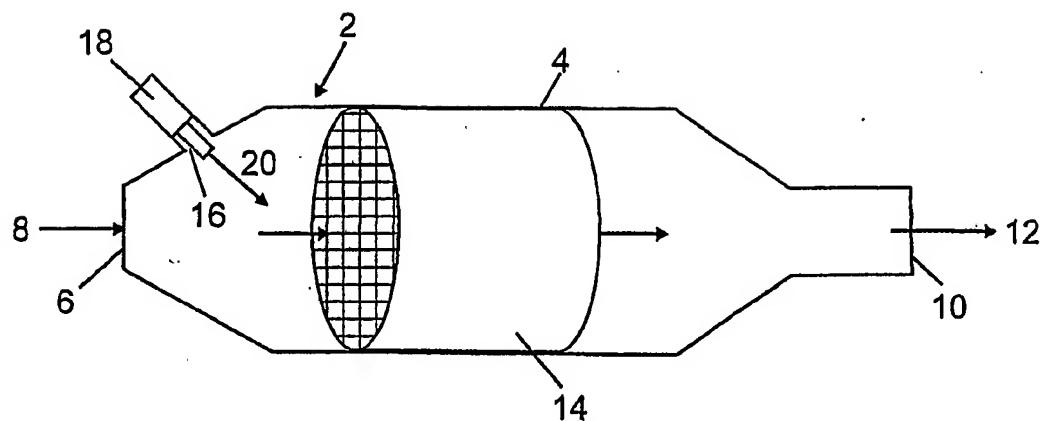


FIGURE 1

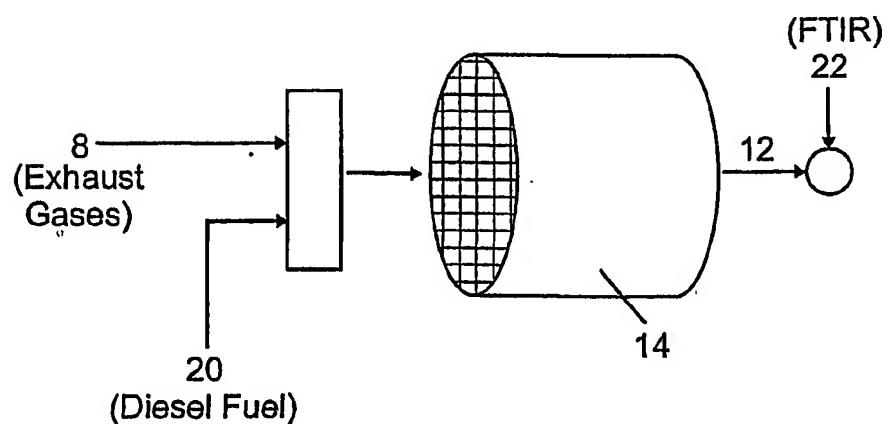


FIGURE 2

## INTERNATIONAL SEARCH REPORT

International application No.

PCT/US01/28907

## A. CLASSIFICATION OF SUBJECT MATTER

IPC(7) : F01N 3/10; 3/20, 3/36; B01J 23/00, 29/00; B01D 53/34, 53/56; 53/94  
 US CL : 422/171, 172, 177, 182, 183; 60/299, 303; 423/213.2, 213.5, 239; 502/232, 302, 303, 324, 350  
 According to International Patent Classification (IPC) or to both national classification and IPC

## B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 422/171, 172, 177, 182, 183; 60/299, 303; 423/213.2, 213.5, 239; 502/232, 243, 244, 259, 263, 302, 303, 313, 324, 350

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched  
NONEElectronic data base consulted during the international search (name of data base and, where practicable, search terms used)  
EAST

## C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US 5,968,464 A (PETER-HOBLYN et al) 19 October 1999, see entire document	1-3, 17-19
—		_____
Y		4-16, 20-32
X	US 5,833,932 A (SCHMELZ) 10 November 1998, see entire document.	1-3, 17-19
—		_____
Y		4-16, 20-32
X	US 5,711,147 A (VOGTLIN et al) 27 January 1998, see entire document.	1-3, 17-19
X	US 5,208,205 A (SUBRAMANIAN et al) 04 May 1993, see entire document.	1-3, 17-19
—		_____
Y		4-16, 20-32
X	US 5,189,876 A (HIROTA et al) 02 March 1993, see entire document.	1-3, 17-19
—		_____
Y		4-16, 20-32

<input type="checkbox"/>	Further documents are listed in the continuation of Box C.	<input type="checkbox"/>	See patent family annex.
* Special categories of cited documents:			
"A"	document defining the general state of the art which is not considered to be of particular relevance	"T"	later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
"B"	earlier application or patent published on or after the international filing date	"X"	document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
"L"	document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)	"Y"	document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
"O"	document referring to an oral disclosure, use, exhibition or other means	"&"	document; member of the same patent family
"P"	document published prior to the international filing date but later than the priority date claimed		

Date of the actual completion of the international search 30 December 2001 (30.12.2001)	Date of mailing of the international search report 13 FEB 2002
Name and mailing address of the ISA/US Commissioner of Patents and Trademarks Box PCT Washington, D.C. 20231 Facsimile No. (703)305-3230	Authorized officer Hien Tran CEROPANTHOMAS PARALEGAL STAFF-137 Telephone No. 308-0661

**INTERNATIONAL SEARCH REPORT**

International application No.

PCT/US01/28907

**Box I Observations where certain claims were found unsearchable (Continuation of Item 1 of first sheet)**

This international report has not been established in respect of certain claims under Article 17(2)(a) for the following reasons:

1.  Claim Nos.: because they relate to subject matter not required to be searched by this Authority, namely:
  
2.  Claim Nos.: because they relate to parts of the international application that do not comply with the prescribed requirements to such an extent that no meaningful international search can be carried out, specifically:
  
3.  Claim Nos.: because they are dependent claims and are not drafted in accordance with the second and third sentences of Rule 6.4(a).

**Box II Observations where unity of invention is lacking (Continuation of Item 2 of first sheet)**

This International Searching Authority found multiple inventions in this international application, as follows:  
Please See Continuation Sheet

1.  As all required additional search fees were timely paid by the applicant, this international search report covers all searchable claims.
2.  As all searchable claims could be searched without effort justifying an additional fee, this Authority did not invite payment of any additional fee.
3.  As only some of the required additional search fees were timely paid by the applicant, this international search report covers only those claims for which fees were paid, specifically claims Nos.:
  
4.  No required additional search fees were timely paid by the applicant. Consequently, this international search report is restricted to the invention first mentioned in the claims; it is covered by claims Nos.: 1-32

**Remark on Protest**  

The additional search fees were accompanied by the applicant's protest.

No protest accompanied the payment of additional search fees.

**INTERNATIONAL SEARCH REPORT**

International application No.

PCT/US01/28907

**BOX II. OBSERVATIONS WHERE UNITY OF INVENTION IS LACKING**

Group I, claim(s) 1-32, drawn to a method for reducing NO<sub>x</sub> and an exhaust gas NO<sub>x</sub> reducing system.

Group II, claim(s) 33-38 and 57-58, drawn to a catalyst composition and a catalytic unit.

Group III, claim(s) 39-41 and 54-56, drawn to another catalyst composition and another catalytic unit.

Group IV, claim(s) 42-45 and 50-53, drawn to another catalyst composition and another catalytic unit.

Group V, claim(s) 46-49 and 59-62, drawn to another catalyst composition and another catalytic unit.

The inventions listed as Groups I-V do not relate to a single general inventive concept under PCT Rule 13.1 because, under PCT Rule 13.2, they lack the same or corresponding special technical features for the following reasons:

The special technical feature Group I is a catalytic reactor having a catalyzed substrate and a fuel injector; while the special technical feature of Group II is a specific perovskite compound;

the special technical feature of Group III is a metal oxide;

the special technical feature of Group IV is a zeolite; and

the special technical feature of Group V is combination of zeolite and metal oxide impregnated with a precious metal (Group V contains claims linking groups III and IV); therefore, holding of lack of unity is proper.